## CE11 Final Exam 2022

## Grading rubric:

| Correct | Sig figs | Unit error | Minor error | Error | Major error | Tried <br> something | No <br> submission |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $-5 \%$ | $-10 \%$ | $-25 \%$ | $-50 \%$ | $-75 \%$ | $-90 \%$ | $-100 \%$ |
|  | -0.1 pts | -0.2 pts | -0.5 pts | -1 pts | -1.5 pts | -1.8 pts | -2 pts |

Correct numerical answers provided without sufficient rationale or justification were graded as a minor error (partial justification) or error (no justification).

## B1. ENERGY BALANCE FOR A FLAT PLANET

Suppose the Earth is really flat. Imagine an Earth that is shaped like a large penny, with one side that directly faces the sun at all times. Also suppose that this flat Earth is the same temperature everywhere, including the side that faces away from the sun. Neglect any radiation losses from the rim (i.e., very thin side edge) of the Earth, and assume there is no albedo or greenhouse effect. Estimate the surface temperature $\mathbf{T}_{\mathrm{E}}$ of this new, flat Earth, assuming an incoming solar radiation intensity $\mathrm{S}_{0}=1360 \mathrm{~W} / \mathrm{m}^{2}$.

The energy entering the system is:
$E_{\text {in }}=S^{*} \pi R^{2}$ (Surface of the disk - one side)

The energy leaving the system is:
$E_{\text {out }}=L^{*} 2 \pi R^{2}$ (Two sides of the disk)
With $L=\sigma T^{4}$

By resolving $E_{\text {in }}=E_{\text {out }}$, we get:
$S * \pi R^{2}=\sigma T^{4} * 2 \pi R^{2}$
$S=\sigma T^{4} * 2$
$T=\sqrt[4]{\frac{S}{2 \sigma}}=331 \mathrm{~K}$

## B2. WORLD SUPPLY OF COBALT

Worldwide reserves of cobalt are estimated to be 7 million metric tons, with a current production rate of 140,000 tons per year. How many years of supply remain assuming production grows exponentially at $3 \%$ per year?

We have $P(t)=P_{0} e^{r t}$
We want to find the number of years after which the aggregate production will be of $Q=7$ million tons.

$$
\begin{aligned}
& \int_{0}^{T} P(t) d t=\int_{0}^{T} P_{0} e^{r t} \\
& Q=\frac{P_{0}}{r}\left(e^{r T}-1\right) \\
& T=\frac{1}{r} \ln \left(\frac{r Q}{P_{0}}+1\right)=\frac{1}{0.03} \ln \left(\frac{0.03^{*} 7 \times 10^{6}}{140,000}+1\right)=31 \text { years }
\end{aligned}
$$

## B3. HEATING VALUE FOR ACETYLENE

Calculate the lower and higher heating values for acetylene $\left(\mathrm{C}_{2} \mathrm{H}_{2}\right)$. Answer in $\mathrm{kJ} / \mathrm{g}$ units. The complete stoichiometric combustion of acetylene is as follows:
$\mathrm{C}_{2} \mathrm{H}_{2}+2.5 \mathrm{O}_{2}+10 \mathrm{~N}_{2} \rightarrow 2 \mathrm{CO}_{2}+1 \mathrm{H}_{2} \mathrm{O}+10 \mathrm{~N}_{2}$
Heats of formation are $\mathrm{C}_{2} \mathrm{H}_{2},+227 \mathrm{~kJ} / \mathrm{mol} ; \mathrm{H}_{2} \mathrm{O}(\mathrm{g}),-242 \mathrm{~kJ} / \mathrm{mol} ; \mathrm{CO}_{2},-394 \mathrm{~kJ} / \mathrm{mol}$. $\mathrm{O}_{2}$ and $\mathrm{N}_{2}$ have zero heat of formation. The heat of vaporization of water is $2.5 \mathrm{~kJ} / \mathrm{g}$.

We sum the different heats of formation accordingly to the stoichiometric coefficients:
$\Delta h_{c}=2 \Delta h_{f, C O_{2}}+\Delta h_{f, H_{2} 0}-\Delta h_{f, C_{2} H_{2}}=2(-394 \mathrm{~kJ} / \mathrm{mol})+(-242 \mathrm{~kJ} / \mathrm{mol})-(227 \mathrm{~kJ} / \mathrm{mol})$
$\Delta h_{c}=-1257 \mathrm{~kJ} / \mathrm{mol}$

We then divide by the molecular weight of acetylene $(2 \times 12+2 \times 1=26 \mathrm{~g} / \mathrm{mol})$
$L H V=\frac{-\Delta h_{c}}{M_{c_{2} H_{2}}}=48.3 \mathrm{~kJ} / \mathrm{g}$

To calculate the HHV, we simply add the heat needed to vapor the water produced during the combustion (here 1 mole of $\mathrm{H}_{2} \mathrm{O}$ is produced for 1 mole of $\mathrm{C}_{2} \mathrm{H}_{2}$ burned):
$H H V=L H V+\frac{M W_{H 2 O}}{M W_{C 2 H 2}} * \Delta h_{v, H 20}=50.0 \mathrm{~kJ} / \mathrm{g}$

## B4. WIND TURBINE EFFICIENCY

An offshore wind turbine with rotor diameter $\mathrm{D}=220 \mathrm{~m}$ delivers its rated power output of 12 MW at wind speeds of $12 \mathrm{~m} / \mathrm{s}$ or higher. For a wind speed of $15 \mathrm{~m} / \mathrm{s}$, calculate the fraction of the available kinetic energy of the air flow past the turbine per unit time that is being converted to electricity. Assume an air density of $1.2 \mathrm{~kg} / \mathrm{m}^{3}$

From the lecture, we know that the available kinetic energy for a $15 \mathrm{~m} / \mathrm{s}$ wind speed is:
$P_{0}=\frac{1}{2} * \pi *\left(\frac{D}{2}\right)^{2} * \rho_{\text {air }} * v^{3}=\frac{1}{2} * \pi *\left(\frac{220}{2}\right)^{2} *\left(1.2 \mathrm{~kg} / \mathrm{m}^{3}\right) *(15 \mathrm{~m} / \mathrm{s})=77 \mathrm{MW}$

Since the wind speed is higher than $12 \mathrm{~m} / \mathrm{s}$, the power output $P=12 \mathrm{MW}$. Therefore:
$\eta=\frac{P}{P_{0}}=16 \%$.

## B5. DRIVING RANGE FOR AN ELECTRIC VEHICLE

Suppose an electric vehicle with a fully-charged 60 kWh battery is driving on a flat level highway at a steady speed of $110 \mathrm{~km} / \mathrm{h}=30.6 \mathrm{~m} / \mathrm{s}$. Estimate the driving range (answer in km ) given relevant data listed below.

Drag Coefficient $\mathrm{C}_{\mathrm{D}}=0.23$
Rolling Resistance Coefficient $\mathrm{C}_{\mathrm{R}}=0.015$
Frontal Area $\mathrm{A}_{\mathrm{F}}=2.2 \mathrm{~m}^{2}$
Vehicle Mass $\mathrm{m}=1800 \mathrm{~kg}$
DC Electric Motor Efficiency $\eta=90 \%$
Transmission Efficiency $\varepsilon=100 \%$
Power to run Air Conditioning $\mathrm{P}_{\mathrm{ACC}}=500 \mathrm{~W}$
Air Density $\rho_{\text {air }}=1.2 \mathrm{~kg} / \mathrm{m}^{3}$

The resistive force for the vehicle is equal to:
$F_{r e s}=C_{d} * A_{f} * \frac{\rho_{a i r}{ }^{*} v^{2}}{2}+C_{r} * m * g=549 N$

The resulting electric power consumption for vehicle propulsion is:

$$
P_{\text {elec, motor }}=\frac{F_{r e s}{ }^{*} v}{\eta^{*} \in}
$$

The total electric power consumption is therefore:

$$
P_{\text {consumed }}=P_{\text {elec, motor }}+P_{A C}=19 \mathrm{~kW}
$$

We then calculate the driving range based on the battery capacity:
Range $=\frac{\text { Battery capacity }}{P_{\text {consumed }}} * v=344 \mathrm{~km}$

## B6. SHELTERING INDOORS TO AVOID FOREST FIRE SMOKE

Suppose outdoor air quality is poor due to smoke from nearby forest fires. Assume the outdoor level of airborne particulate matter (PM) is $150 \mu \mathrm{~g} / \mathrm{m}^{3}$. Consider a home with V $=400 \mathrm{~m}^{3}$ and an air exchange rate $\mathrm{Q} / \mathrm{V}=0.5 \mathrm{hr}^{-1}$. There are no indoor sources of smoke, and the initial concentration of smoke indoors is zero. Calculate the indoor PM concentration, one hour after the outdoor air starts to be significantly polluted by forest fire smoke. Assume there are no air purifiers or filters indoors. Answer in $\mu \mathrm{g} / \mathrm{m}^{3}$ units.

The variation of concentration is given by:
$V \frac{d C}{d t}=Q C_{\text {out }}-Q C$
$\frac{d C}{d t}=\frac{Q}{V}\left(C_{\text {out }}-C\right)$
$\frac{d C}{C_{\text {out }}-C}=\frac{Q}{V} d t$
$-\ln \left(\frac{C-C_{\text {out }}}{-C_{\text {out }}}\right)=\frac{Q}{V} t$
$C-C_{\text {out }}=-C_{\text {out }} e^{-\frac{Q}{V} t}$

We therefore have:
$C=C_{\text {out }}\left(1-e^{-\frac{Q}{V} * t}\right)=59 \mu \mathrm{~g} / \mathrm{m}^{3}$

## B7. FILTERING INDOOR AIR

Suppose for the same house as in the previous question, there is an air filter operating with a flow rate of $\mathrm{Q}_{\mathrm{F}}=2000 \mathrm{~m}^{3} / \mathrm{hr}$ and a filtration efficiency of $80 \%$ that removes smoke particles from indoor air. What will be the steady state concentration of PM indoors? Give your answer in $\mu \mathrm{g} / \mathrm{m}^{3}$ units.

The steady state equation in this situation is given by:
$C_{\text {out }} * Q=C_{\text {steady }} * Q+C_{\text {steady }} * Q_{F}^{*} \eta=C_{\text {steady }}\left(Q+Q_{F} * \eta\right)$

We therefore have:

$$
C_{\text {steady }}=\frac{C_{\text {out }}}{1+\frac{Q_{F}}{Q} \eta}
$$

$$
C_{\text {steady }}=\frac{C_{\text {out }}}{1+\frac{Q_{F} * \frac{v^{*}}{V}}{Q} \cdot \eta}=17 \mu \mathrm{~g} / \mathrm{m}^{3}
$$

## B8. MITIGATING HYDROGEN SULFIDE ODOR

Hydrogen sulfide $\left(\mathrm{H}_{2} \mathrm{~S}\right)$ is a foul-smelling gas that is soluble in water. One odor mitigation strategy involves altering the pH of water to reduce the amount of dissolved sulfur present in volatile $\left(\mathrm{H}_{2} \mathrm{~S}\right)$ form. Assume the only important dissolved forms are undissociated $\mathrm{H}_{2} \mathrm{~S}$ and the bisulfide ion, $\mathrm{HS}^{-}$. The dissociation reaction is

$$
\mathrm{H}_{2} \mathrm{~S} \Leftrightarrow \mathrm{HS}^{-}+\mathrm{H}^{+} \quad \text { with } K_{A 1}=\frac{\left[H S^{-}\right]\left[H^{+}\right]}{\left[H_{2} S\right]}=10^{-7.1}
$$

Calculate and compare the fraction of total dissolved sulfur present in $\mathrm{H}_{2} \mathrm{~S}$ form at $\mathrm{pH}=7$ and $\mathrm{pH}=8$.

The definition of pH is:
$p H=-\log \left[H^{+}\right] \Leftrightarrow\left[H^{+}\right]=10^{-p H}$

The fraction of H 2 S is equal to:
$c_{H_{2} S, p H}=\frac{\left[H_{2} \mathrm{~S}\right]}{\left[H_{2} \mathrm{~S}\right]+\left[H S^{-}\right]}=\frac{1}{1+\frac{\left[H S^{-}\right]}{\left[H_{2}\right]}}$

And we know from the dissociation reaction equation that:
$\frac{\left[H^{+}\right]\left[H S^{-}\right]}{\left[H_{2}\right]}=K_{A 1} \Leftrightarrow \frac{\left[H S^{-}\right]}{\left[H_{2} S\right]}=\frac{K_{A 1}}{\left[H^{+}\right]}$with $\mathrm{K}_{\mathrm{A} 1}=10^{-7.1}=7.9 \times 10^{-8} \mathrm{~mol} / \mathrm{L}$

By using the definition of pH , we therefore have:
$\frac{\left[\mathrm{HS}^{-}\right]}{\left[\mathrm{H}_{2} \mathrm{~S}\right]}=\frac{K_{A 1}}{10^{-p H}}$
$c_{H_{2} S, p H}=\frac{1}{1+\frac{K_{K_{11}}}{10^{p+1}}}$

We then calculate the values for $\mathrm{pH}=7$ and $\mathrm{pH}=8$.
$c_{H_{2} S, p H=7}=56 \%$
$c_{H_{2} S, p H=8}=11 \%$

We therefore prefer a pH of 8 as the fraction of total dissolved sulfur present as $\mathrm{H}_{2} \mathrm{~S}$ (the volatile form) is lower in this situation.

## B9. DISSOLVED OXYGEN IN A RIVER

Suppose deoxygenation and reaeration rate coefficients in a river are equal, $\mathrm{k}=$ $0.3 /$ day. Given an initial dissolved oxygen deficit of $3 \mathrm{mg} / \mathrm{L}$, and an ultimate oxygen demand of $10 \mathrm{mg} / \mathrm{L}$ for water in the river just downstream of an effluent discharge, calculate the maximum value for the dissolved oxygen deficit downstream (answer in $\mathrm{mg} / \mathrm{L}$ ).
From the lecture, we know that the deficit is equal to $D(t)=\left(k L_{0} t+D_{o}\right) e^{-k t}$.
We can thus calculate the derivative of D :
$\frac{d D}{d t}=k L_{0} e^{-k t}-\left(k L_{0} t+D_{0}\right) * k e^{-k t}=k e^{-k t} *\left(L_{0}-L_{0} k t+D_{0}\right)$

We then want to find the maximum of $D$ which is reached for:
$\frac{d D(t)}{d t}=0 \Leftrightarrow L_{0}\left(1-k t_{c}\right)+D_{0}=0 \Leftrightarrow t_{c}=\frac{L_{0}-D_{0}}{k L_{0}}=2.3$ days

We finally simply have to plug this value in the initial $D$ formula:
$D\left(t_{c}\right)=5.0 \mathrm{mg} / L$

## B10. UNCERTAINTY ANALYSIS

Given a measured value $x=4.0 \pm 0.2$, estimate the resulting uncertainty in $y=x^{3}$. In other words, what is the appropriate value for $\sigma_{\mathbf{y}}$ in the calculated result $y=64 \pm$ $\sigma_{\mathrm{y}}$ ?
$y=f(x)=x^{3}$
$\frac{d f}{d x}=3 x^{2}$
$\sigma_{y}^{2}=\left(\frac{d f}{d x} * \sigma_{x}\right)^{2}$
$\sigma_{y}=\left|\left(3 x^{2}\right) * \sigma_{x}\right|=48 \times 0.2=9.6$

